

1 **Synthesis and characterization of alginate-polyacrylic acid/multiwalled**
2 **carbon nanotubes composite with efficient removal for nigrosine dye**

3 Mohamed I. A. Ibrahim^{a,b*}, Islam M. Abdelmonem^c, Laila A. Mohamed^a,
4 Mohamed A. Gizawy^d, E. Metwally^c

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6 *^aNational Institute of Oceanography and Fisheries, NIOF, Egypt.*

7 *^bHiroshima Synchrotron Radiation Center, Hiroshima University, Kagamiyama,*
8 *Higashi-Hiroshima, Hiroshima 739-0046, Japan*

9 *^cNuclear Chemistry Department, Hot Labs Center, Egyptian Atomic Energy Authority,*
10 *P.O. Box 13759, Cairo, Egypt.*

11 *^dLabeled Compounds Department, Hot Labs Center, Egyptian Atomic Energy Authority,*
12 *P.O. Box 13759, Cairo, Egypt.*

13 *Corresponding Author

14 Mohamed I. A. Ibrahim

15 Assistant professor of Marine Chemistry,

16 Laboratory of Marine Chemistry, National Institute of Oceanography and Fisheries,
17 NIOF, Egypt.

18 Hiroshima Synchrotron Radiation Center, HiSOR, Hiroshima University, Japan.

19 Tel: +2-03-480-1553 / +81-82-424-6293

20 Fax: +2-03-480-1449 / +81-82-424-6294

21 ORCID: 0000-0001-6190-5899

22 Scopus Author ID: 57195522700

23 E. mail: ibrahimmohamed2030@gmail.com

24 m.ibrahim@niof.sci.eg

25 ibra2020@hiroshima-u.ac.jp

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27 **Synthesis and characterization of alginate-polyacrylic acid/multiwalled**
28 **carbon nanotubes composite with efficient removal for nigrosine dye**

29 **Abstract:** The current study detailed the efficacy of a simply prepared alginate-
30 polyacrylic acid/functionalized multiwalled carbon nanotubes (Alg-PAA/f-
31 MWCNTs) composite for adsorption of nigrosine dye (acid black II) from
32 aqueous environments. Firstly, preparation of the Alg-PAA/f-MWCNTs
33 composite was achieved *via* gamma radiation-induced template
34 polymerization of AA onto the Alg/f-MWCNTs surface. The maximum
35 grafting efficiency (GE%) of AA onto the surface of Alg/f-MWCNTs was ~
36 82% under the optimized conditions: (2.5 wt% Alg, 30 wt% AA, 0.5 wt% f-
37 MWCNTs, 0.6 wt% *N,N'*-methylenebisacrylamide (NMBA), and irradiation
38 dose ~ 20 kGy). The structural characteristics, thermal features as well as the
39 morphological appearance of the Alg-PAA/f-MWCNTs composite were
40 validated using different analyses including FTIR, TGA, DTA, XRD and
41 SEM. Additionally, the composite exhibited uniform particle size distribution
42 (~ 150.7 nm), point of zero charge at pH = 6.28, and negative Zeta potentials
43 of a minimum at pH = 2. The adsorption batch experiments showed good
44 adsorption capacity for the nigrosine dye from their aqueous media with
45 adsorption efficiency up to 83% using the batch technique at pH = 2.0 for 420
46 min. The adsorption of nigrosine dye onto Alg-PAA/f-MWCNTs is
47 favourable thermodynamically, obeying the Freundlich isotherm model and
48 controlled by a chemisorption mechanism. Additionally, the composite
49 showed a good regeneration ability up to five times with almost the same
50 removal % (~ 80%). The results demonstrated that the Alg-PAA/f-MWCNTs
51 composite could be a promising candidate for the removal of nigrosine dye
52 from industrial aqueous environments.

53

54 **Keywords:** biosorption; nigrosine; alginate-polyacrylic acid/multiwalled
55 carbon nanotubes; kinetics; thermodynamics

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58

59 **Introduction**

60 Recently, synthetic dyes have been widely utilized in many processing industries (e.g.,
61 inks, textiles, cosmetics, rubbers, plastics, leather, papers, food, etc.).^[1, 2] Dyes are
62 classified into anionic dyes, cationic dyes, and non-ionic ones of dispersed behaviours.^[3]
63 The majority of the dyes are of synthetic origin, possessing complex structures, which
64 make them more stable and less biodegradable. Because of their high solubility and
65 toxicity, dyes are an influential source of water pollutants even at low concentrations (<
66 1.0 ppm),^[4] which adversely affect the aquatic life and food web. Several studies have
67 offered the removal of dyes from wastewaters. Numerous physical methods have been
68 reported to reduce the hazard effects of the dye effluents such as reverse osmosis, ultra-
69 filtration, ion exchange, coagulation and flocculation, photo-degradation, and
70 adsorption.^[5-7] Furthermore, several chemical processes such as photosensitized
71 oxidation, adsorption, and photofenton's reactions have also been applied for removing
72 dyes.^[8-11] However the aforementioned methods are fairly effective in pollutants'
73 removal, most of them suffer from transforming the dyes solution into solid forms which
74 need further treatment. Among all methods, adsorption is considered as one of the
75 promising and effective ways for removing dyes from polluted waters, producing waters
76 of high quality. Adsorption principle has been successfully applied for the removal of
77 several dyes including methylene blue (MB), rhodamine B, methyl orange, congo red,
78 acid black II, disperse violet 26, methyl red, and crystal violet (CV), from wastewaters
79 originating particularly from textile, cosmetic, leather, food, pharmaceutical, paint and
80 varnish, pulp, and paper industries.^[12-16]
81 Many studies highlighted the use of bio-sorbents (e.g., starch, alginate, chitin, chitosan,
82 etc.) for removing dyes from wastewaters as eco-friendly, cost-effective, and
83 commercially available adsorbents. Biopolymers are distinguished of being naturally

84 abundant, biodegradable, biocompatible, and exhibiting versatile chemical structures
85 associated with the presence of various active functional groups, which contribute
86 effectively towards the removal of dyes.^[17] Unfortunately, biopolymers have been limited
87 in various applications due to their weak mechanical properties, or gel formation.
88 Additionally, natural polymers are not sufficient to remove the dyes from highly complex
89 dye-containing wastewaters contaminated with different types of pollutants. To overcome
90 limitations, the biopolymers should be subjected to a modification process, involving
91 chemical or physical strategy, to increase their efficiency in removing dyes from complex
92 wastewaters.^[18] Radiation-induced graft polymerization offers a convenient method for
93 modifying polymers, introducing new characteristics while preserving the original ones.
94 Various radiation sources, such as electron beams, UV, and γ -radiation, can be employed
95 for this process.^[19] When ionizing radiation interacts with matter, particularly through the
96 atomic shell's electrons, it generates reactive species, predominantly free radicals, leading
97 to ionization or excitation.^[20] The advantages of radiation-induced graft polymerization
98 include its simplicity, the ability to control graft content and reaction parameters, and
99 compatibility with commercially available polymer substrates. Additionally, this method
100 avoids the use of potentially hazardous materials such as catalysts, additives, initiators,
101 or organic solvents.^[21, 22] Poly(ethersulfone) membranes underwent surface modification
102 through a straightforward one-step process. The membranes were immersed in aqueous
103 solutions containing diverse low-molecular-weight molecules with varied hydrophilic
104 functionalities, followed by electron beam treatment.^[23] Gamma irradiation crosslinking
105 was also applied to prepare polyacrylic acid-polyvinyl alcohol-polyethylene oxide
106 [p(AAc/PVA/PEO)] hydrogel membranes. This process creates a three-dimensional
107 network structure, or hydrogel, by creating chemical links between polymer chains.^[24]

108 Alginate, a naturally occurring anionic polymer, has been extensively researched and
109 applied in various biomedical contexts due to its attributes of low toxicity,
110 biocompatibility, and cost-effectiveness^[25]. On the other hand, multi-walled carbon
111 nanotubes (MWCNTs) have garnered a significant attention as additives, given their
112 unique capabilities in adsorption, catalysis, thermal conductivity, mechanical strength,
113 and electrical conductivity.^[26] The process of functionalizing MWCNTs enhances their
114 reactivity, solubility, and opens new avenues for chemical modification. Moreover, the
115 introduced functional groups serve as anchor points, facilitating the bonding of two
116 entities and enabling further derivatization through chemical interactions with additional
117 functional groups.^[27] Thus, alginate-based composites have been extensively researched
118 for the removal of synthetic dyes from aqueous solution. Benhouria et al. (2015)
119 developed bentonite-alginate beads to eliminate methylene blue, achieving a maximum
120 monolayer adsorption capacity of 756.97 mg/g at 30°C after six regeneration cycles.^[28]
121 Fan et al. (2013) synthesized graphene oxide/sodium alginate/polyacrylamide
122 (GO/SA/PAM) composite hydrogels, which effectively adsorb cationic and anionic dyes
123 from wastewater.^[29] Sui et al. (2012) studied ionic dye adsorption on calcium alginate
124 and multi-walled carbon nanotube (CA/MWCNT) composite fibers, finding MWCNTs
125 increased the adsorption capacity and improved the removal rate.^[30] Wang, Wang, and
126 Wang (2013) developed NaAlg-g-p(AA-co-St)/organo-I/S nanocomposite absorbents to
127 eliminate MB, achieving a fast adsorption capacity of 1843.46 mg/g.^[31]
128 Nigrosine dye (acid black II) is an anionic azo dye, a mixture of black dyes (i.e., CI 50415,
129 and solvent black 5), synthesized by heating a mixture of aniline, nitrobenzene, and
130 aniline hydrochloride in presence of copper or iron as a catalyst. The sulfonated form of
131 nigrosine dye is more soluble in water and often used for dyeing textiles, leather, and as
132 marker-pen inks as well as in the biology field for negative staining bacteria.^[10, 32] The

133 choice of nigrosine acid black II as the model dye is related that it is a traditional water-
134 soluble dye, in addition to being used as a common analytical reagent. Consequently, a
135 significant amount of nigrosine dye as wastewater is discharged into aquatic
136 environments from laboratories, factories, etc. The current study is one of rare work that
137 focused on the removal of a traditional nigrosine dye from an aqueous solution using a
138 simply designed Alg-PAA/f-MWCNTs composite. Firstly, the composite was prepared
139 through the gamma radiation-induced polymerization of AA onto the Alg/f-MWCNT
140 surface, followed by the structural validation of the composite using FTIR, SEM, TGA,
141 XRD and DTA. Then, the factors affecting the nigrosine removal *via* the adsorption
142 process (e.g., pH, time, nigrosine concentration, and temperature) were examined using
143 batch methods. Modelling of the kinetics, equilibrium isotherms, thermodynamics, and
144 regeneration of the prepared composite were also investigated.

145 **Material and methods**

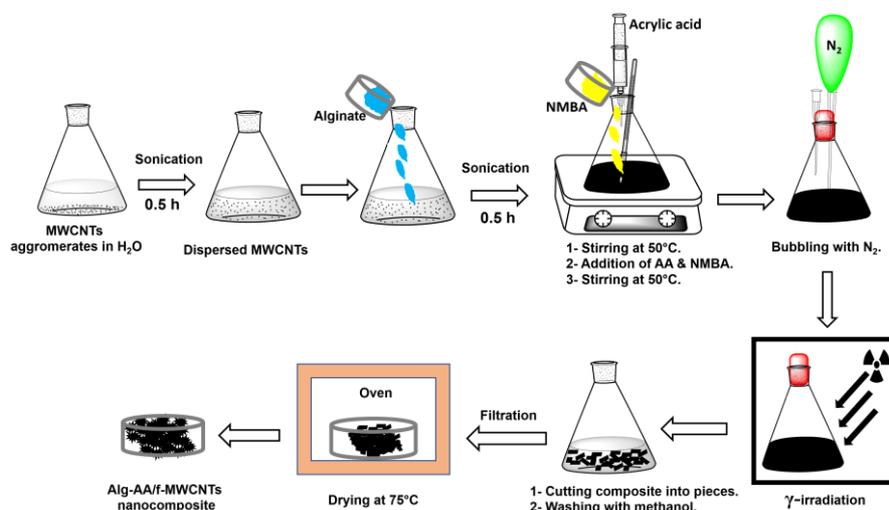
146 *General*

147 All chemicals and solvents of highest purity grades were used in performing the synthesis
148 and experimental part: sodium alginate (Alg; Sigma-Aldrich, Germany), acrylic acid
149 monomer (AA; Merck-Schuchardt, Germany), multi-walled carbon nanotube
150 (MWCNTs; EMFUTUR, Spain), and *N,N'*-methylenebisacrylamide (NMBA; Merck,
151 Germany).

152 *Synthesis of the Alg-PAA/f-MWCNTs composite*

153 The Alg-PAA/f-MWCNTs composite was synthesized through multiple consecutive
154 steps in a good overall yield as illustrated in **Figure 1**. Firstly, chemical oxidation of the
155 MWCNTs was carried out using a strategy described elsewhere.^[26, 33] The yielded f-
156 MWCNTs were ultrasonicated in distilled water for 0.5 h before the addition of sodium
157 alginate, and the suspension was heated at 50°C until a homogeneous solution was

158 obtained. Afterward, AA then NMBA (crosslinker) were added to the solution under
 159 agitation at 50°C until homogeneity was observed.



160

161 **Figure 1.** Schematic representation of a stepwise procedure for the synthesis of Alg-
 162 PAA/f-MWCNTs.

163 The mixture was bubbled with nitrogen gas to discard the oxygen before subsection to
 164 polymerization by γ -radiation. The polymerization was achieved at ambient temperature
 165 using γ -radiation with an average dose rate of ~ 1.05 kGy/h using a ^{60}Co - γ -ray field to
 166 reach the optimum radiation dose (Cobalt-60 gamma cell MC-20, Cyclotron Project,
 167 Inshas, Egypt). Finally, the obtained nanocomposites were divided into tiny pieces then
 168 washed with methanol, and the resultant grafted material (Alg-PAA/f-MWCNTs) was
 169 filtered and dried at 75°C till a constant weight was obtained, then was stored for later
 170 evaluations.^[34]

171 The grafting percentage and grafting efficiency were computed using formulas (1) and
 172 (2), respectively.^[35]

173
$$\text{Grafting percentage (G\%)} = \frac{(W_g - W_o)}{W_o} \times 100 \quad \text{Eq. (1)}$$

174
$$\text{Grafting efficiency (GE\%)} = \frac{(W_g - W_o)}{W_m} \times 100 \quad \text{Eq. (2)}$$

175 Where W_o , W_g , and W_m are the weights of polymer backbone (Alg/f-MWCNTs), graft
 176 polymer (Alg-PAA/f-MWCNTs), and monomer (AA), respectively.

177 ***Characterization of the Alg-PAA/f-MWCNTs composite***

178 The structural features of the synthesized Alg-PAA/f-MWCNTs composite were
179 emphasized by Fourier transform infrared (FTIR), thermogravimetric (TGA) and
180 differential thermal analyses (DTA), X-ray diffraction (XRD) analysis (D₂ Phaser-
181 Bruker, Germany), as well as scanning electron microscope (SEM). The chemical
182 functionality of the nanocomposite was identified using FTIR in the range (4000 – 400
183 cm⁻¹) with 4 cm⁻¹ resolution by KBr disc method using a Shimadzu infrared spectrometer
184 (BOMEM, FTIR, Japan). The thermal analyses of the composite using the TGA and DTA
185 involved heating the composite at a rate of 20°C/min (Shimadzu DTG-60 thermal
186 analyzer, Japan). The microstructure morphology of the composite surface was
187 investigated using a scanning electron microscope (JEOL-JSM 6510 LA, Japan).
188 Additionally, the Zeta potential analysis and particle size distribution of composite were
189 determined (Malvern Zeta nano-sizer ZSP ZEN 5600).

190 ***Adsorption studies***

191 ***Preparation of acid black II dye solution***

192 A stock of acid black II dye solution (1000 mg/L) was prepared by dissolving 1.0 g of
193 dye in 1.0 L deionized water. Standard solutions of acid black II dye (5.0,10.0,15.0, and
194 20.0 mg/L) were prepared by diluting (0.25, 0.5, 0.75, and 1.0 mL) of acid black II stock
195 solution into a 50 mL measuring flask and completed to mark with deionized water.

196 ***Batch adsorption experiments***

197 The reaction mixture was prepared by adding exact weights of the adsorbent into 50 mL
198 glass bottles containing 25 mL of the prepared solution. All experiments were carried out
199 using a digital laboratory orbital shaker machine to get the optimum conditions (pH,
200 contact time, dye concentration, and temperature). The samples were filtered for
201 separation of adsorbent. The residual concentrations of dye were measured by a UV-

202 Visible spectrophotometer at a wavelength of 573 nm. The removal percentage of acid
203 black II dye was calculated using equation (3),^[36]

$$204 \quad \% \text{ Removal} = \frac{(C_o - C_e)}{C_o} \times 100 \quad \text{Eq. (3)}$$

205 While (C_o) and (C_e) are the concentrations (mg/L) of the dye at zero time ($t = 0$) and
206 equilibration time (t), respectively. The adsorption capacity of (Alg-PAA/f-MWCNTs)
207 composite at equilibrium Q_e (mg/g) was calculated from equation (4),^[37]

$$208 \quad Q_e = \frac{(C_o - C_e) V}{m} \quad \text{Eq. (4)}$$

209 Where C_e is the equilibrium concentrations of dye (mg/L), V is the volume of the solution
210 (L) and m is the mass of adsorbent (g).

211 *Effect of the adsorption parameters on the removal of dyes*

212 *pH of solution*

213 The effect of pH on Alg-PAA/f-MWCNTs composite was studied by adjusting the acid
214 black II solutions at different values (pH = 2.0 to 12.0), using 0.05 g as adsorbent dose.

215 The experiment was performed at an agitation rate of 200 rpm for 420 min at room
216 temperature, and an initial dye concentration of 10 mg/L, to obtain the pH value of the
217 highest efficient capacity. The initial pH values of aqueous solutions were adjusted by
218 using HCl (0.1 M) or NaOH (0.1 M) solutions, and fresh solutions were prepared for each
219 experiment.

220 The point of zero charge of the prepared composite was also determined. In brief, about
221 0.05 g of the composite was added to an array of 125 stoppered bottles. A 50 mL of
222 different pH buffer solutions (pH = 1.0 – 12.0) were poured into the stoppered bottles
223 under shaking at 200 rpm at room temperature. The pH of the solutions was controlled
224 using 1.0 N HCl, 1.0 N NaOH and acetate buffer. Then, the pH of each bottle was
225 measured using pH meter after 24 hrs. The pH difference (ΔpH) between the initial and

226 final values were calculated using the equation: $\Delta pH = pH_{Initial} - pH_{Final}$ which then
227 plotted against the $pH_{Initial}$. The point of zero charge (pH_{pzc}) of the composite is the pH
228 corresponds to $\Delta pH = zero$.^[38]

229 *Contact time*

230 For determination of the optimum contact time, the adsorption capacities of the Alg-
231 PAA/f-MWCNTs composite for acid black II dye was tested at time intervals (30, 60, 90,
232 120, 180, 360, 420, 960, and 1440 min), agitation speed (200 rpm), pH 2.0, adsorbent
233 dose (0.05 g), and initial dye concentration 10.0 mg/L at room temperature.

234 *Initial dye concentration*

235 The optimum initial dye concentration was determined by evaluating the adsorption
236 capacities of the composite towards the dye at various concentrations (0.5, 1.0, 2.0, 5.0,
237 10, 15, 20, 50, and 100 mg/L) at constant agitation speed (200 rpm), pH 2.0, adsorbent
238 dose (0.05 g), during agitation time of 420 min at room temperature.

239 *Temperature*

240 The experiments help to follow the adsorption extents of acid black II dye on the
241 composite surfaces with temperature variations. The experiments were performed using
242 an initial dye concentration of 10 mg/L at five different temperatures (30, 40, 50, and 60
243 °C), agitation speed (200 rpm), pH 2, and adsorbent dose (0.05 g) for 180 min.

244 ***Adsorption kinetics, isotherm, and thermodynamics***

245 Adsorption kinetics were modeled and compared using pseudo-first-order (PFO), pseudo-
246 second-order (PSO), and the intraparticle diffusion model (IPD) (Weber and Morris
247 model). On the other side, adsorption isotherms were modeled using Langmuir,
248 Freundlich and Temkin models. Adsorption thermodynamics parameters [e.g., Gibbs free

249 energy (ΔG° , kJ/mol), enthalpy change (ΔH° , kJ/mol), entropy change (ΔS° , J/mol/K)]
 250 were determined using Van't Hoff equation.

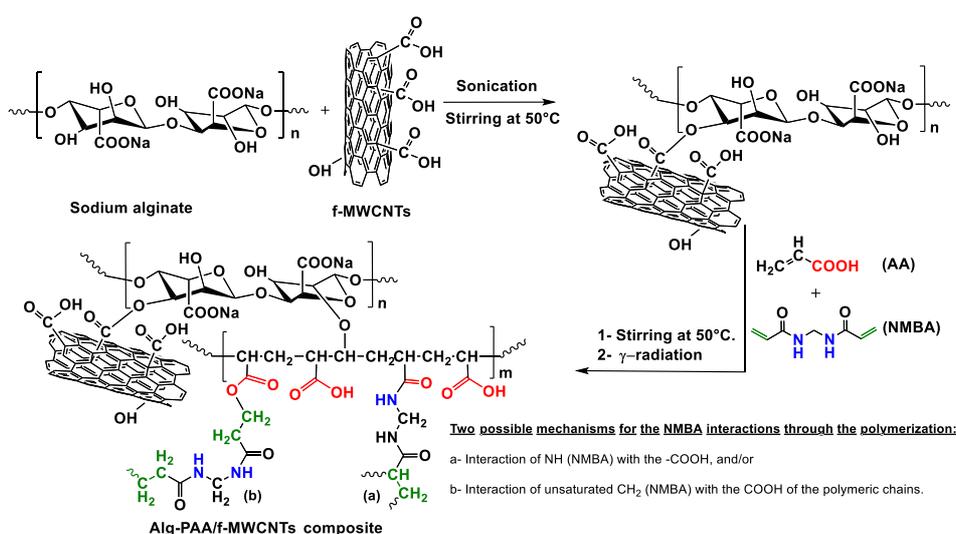
251 **Regeneration of adsorbent**

252 The reusability of the adsorbent, desorption test, was carried out at 25°C (pH 2.0, $C_0 = 10$
 253 mg/mL, $t = 420$ min, and adsorbent dose = 0.05 g) for five consecutive cycles. The acid
 254 black II dye bound to the Alg-PAA/f-MWCNTs was exposed to a 25 mL solution with a
 255 pH of 12, allowed to reach equilibrium, subjected to filtration, and subsequently analyzed
 256 for its dye concentration in the filtrate. After desorption, the Alg-PAA/f-MWCNTs were
 257 washed with ultrapure water for the next adsorption cycle.

258 **Results and discussion**

259 **Synthesis of the Alg-PAA/f-MWCNTs composite**

260 The overall stepwise synthesis of the Alg-PAA/f-MWCNTs composite is illustrated in
 261 **Figure 2** with some modifications of the previously reported protocol.^[26, 33, 39] The
 262 MWCNTs were functionalized through oxidation steps, creating hydroxyl (-OH) and
 263 carboxyl (-COOH) groups as active sites for reacting with the hydroxyl (-OH) groups of
 264 the alginate moieties.



265

266 **Figure 2.** The general strategy for the synthesis of Alg-PAA/f-MWCNTs composite.

267 Grafting of AA onto the Alg/f-MWCNTs was initiated using γ -radiation by template
268 polymerization technique in the presence of NMBA as a crosslinker. Indeed, two possible
269 mechanisms for the NMBA interactions during polymerization: interaction of the NH
270 group and/or the unsaturated $-\text{CH}_2$ group (NMBA) with the $-\text{COOH}$ groups within the
271 polymeric chains.^[40] The stepwise synthesis and the proposed structure for the novel Alg-
272 PAA/f-MWCNTs composite is presented in **Figure 2**. The mechanism of grafting AA
273 monomers onto Alg/f-MWCNTs surface by γ -radiation-induced polymerization starts when
274 the high-energy γ -rays interact with AA monomeric units, forming free radicals or other
275 reactive species. This process can be initiated through breaking covalent bonds within
276 AA monomers. The free radicals then react with other AA monomeric units, causing
277 chain propagation, which adds monomers to the growing chain, creating longer chains.
278 The process can terminate through reactions between chains or radical recombination,
279 leading to the end of chain growth. The high energy of γ -rays allows for efficient
280 initiation, and the resulting polymers may exhibit unique properties depending on
281 radiation dose and conditions.^[41, 42]

282 The optimized conditions for yielding the highest grafting percentage, grafting efficiency,
283 and swelling degree were established through studying the influence of the AA, Alg,
284 NMBA (crosslinker), and the f-MWCNTs concentrations.

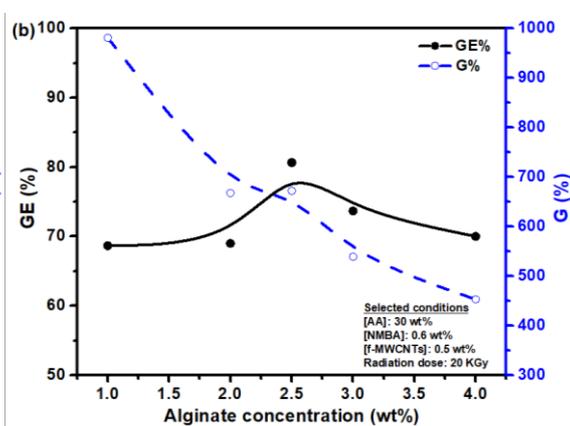
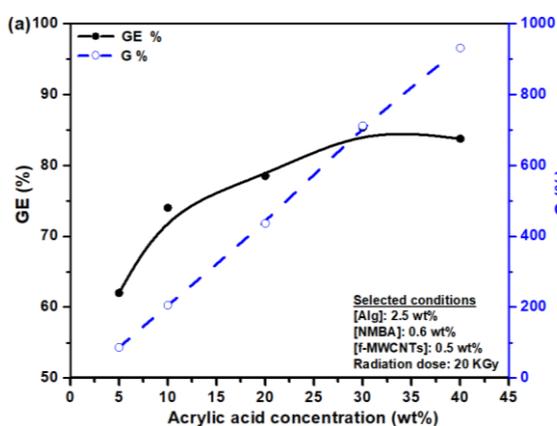
285 ***Optimization conditions for the synthesis of the Alg-PAA/f-MWCNTs composite***

286 Studying the effects of the AA, Alg, NMBA, and f-MWCNTs concentrations on the
287 grafting efficiency (GE%), are the most effective factors in establishing the ideal
288 conditions for the production of the Alg-PAA/f-MWCNTs composite.^[43, 44]

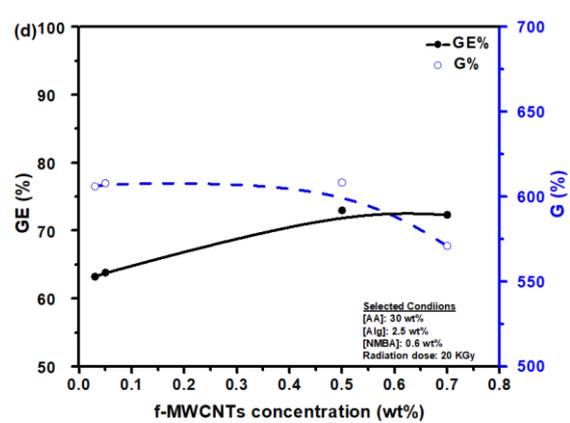
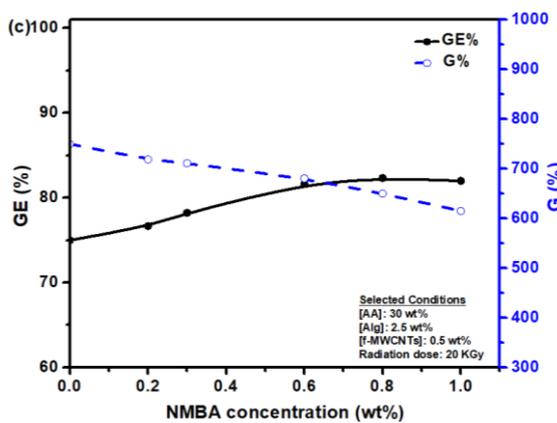
289 *Influence of AA concentration*

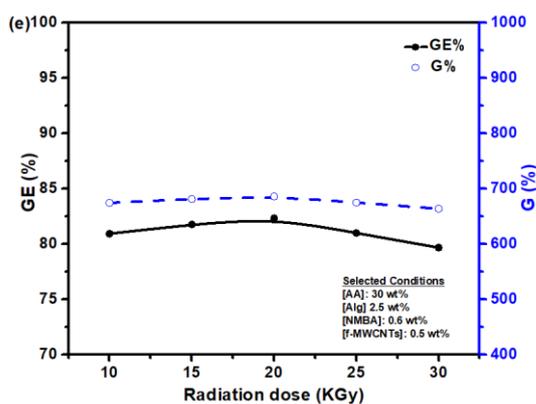
290 The influence of the AA concentrations on the grafting percentage, grafting efficiency,
 291 and swelling degree (S) was studied using a concentration range from 5.0 to 40 wt%, at
 292 fixing the concentrations of other parameters (**Figure 3a**). It has been found that G% and
 293 GE% were increased while AA concentration increased from 5.0 to 30 wt%, which is
 294 associated with the releasing of many free radicals, generating more propagation chains,
 295 and the high availability of AA monomers for grafting. The maximum GE% was 85.3 at
 296 30 wt% for AA. The swelling degree was found to be in the range between 1.5 and 4.66.

297



298





299

300 **Figure 3.** Effect of (a) AA, (b) Alg, (c) NMBA, (d) f-MWCNTs concentrations, and (e)
 301 radiation dose on the grafting percentage (G%) and grafting efficiency (GE%).

302 *Influence of alginate concentration*

303 The effect of Alg concentration on the swelling degree, grafting percentage and efficiency
 304 was carried out using the Alg concentration range of 1.0 – 4.0 wt% at 30 wt% AA, 0.6
 305 wt% NMBA, 0.5 wt% f-MWCNTs, and a radiation dose of 20 kGy. **Figure 3b** shows
 306 that the GE% increased with increasing the Alg concentration from 1.0 to 2.5 wt%. This
 307 finding was explained by the availability of more sites for the initiating the
 308 polymerization process. Beyond 2.5 wt%, the G% and GE% decreased with increasing
 309 the Alg concentration, which was attributed to increasing the reaction medium viscosity,
 310 hindering the diffusion of reactive monomers in the system to interact with the growing
 311 polymeric chains. Thus, the maximum GE% was 80.6% at 2.5 wt% of Alg concentration,
 312 while the swelling degree was found to be from 1.8 to 5.8.

313 *Influence of NMBA concentration*

314 The effect of NMBA concentration on G%, GE%, and the swelling degree was
 315 investigated in the NMBA concentration range from 0.0 to 1.0 wt% at the optimized values
 316 of other components (2.5 wt% Alg, 30 wt% AA, 0.5 wt% f-MWCNTs and 20 kGy
 317 radiation dose) (**Figure 3c**). The G% and GE% increased with increasing the percentage

318 of crosslinker till 0.6 wt%, which may be due to increasing the free radicals generated
319 from NMBA for generating propagation chains. The decrease in G% was observed while
320 the NMBA concentration exceeded 0.6 wt%, which may be due to a higher extent of the
321 crosslinking between the polymeric chains and NMBA.^[45] As a consequence, the
322 probability of monomers' interaction with the added template polymer decreased. The
323 swelling degree was ranged between 0.9 and 4.1.

324 *Influence of f-MWCNTs concentration*

325 The effect of f-MWCNTs concentration on the G%, GE%, and the swelling degree was
326 studied in the concentration range from 0.03 to 0.7 wt%, at the optimized conditions of
327 2.5 wt% Alg, 30 wt% AA, 0.6 wt% NMBA and 20 kGy radiation dose (**Figure 3d**). The
328 GE% and G% increased with increasing the f-MWCNTs concentration to a maximum
329 values of 0.7 wt% and 0.5 wt% respectively, due to the presence of the active groups
330 (e.g., -OH and -COOH) that act as grafting sites on the f-MWCNTs surface^[46]. While a
331 slight decrease in the G% was noticed upon increasing the f-MWCNTs concentration
332 greater than 0.5 wt%, associated with the saturation of active sites. The swelling degree
333 was found to be in the range 3.21 - 6.12.

334 *Influence of radiation dose*

335 The effect of radiation dose on the G%, GE%, and the swelling degree was investigated
336 using the radiation doses from 10 to 30 kGy at 2.5 wt% Alg, 30 wt% AA, 0.6 wt% NMBA,
337 and 0.5 wt% of f-MWCNTs (**Figure 3e**). It was found that G% and GE% slightly
338 increased as the radiation dose increased due to increasing the generated free radicals.
339 The G% and GE% slightly decreased with further increase in the absorbed dose, which
340 may be related to increasing the medium viscosity, hindering the monomers diffusion in

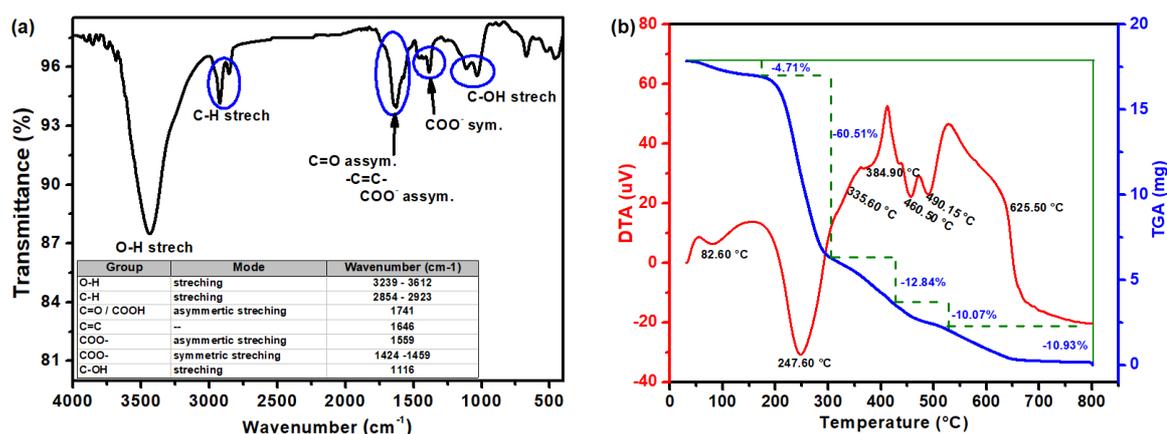
341 the system.^[47] The maximum efficiency (GE%) was 82.33% at a radiation dose of 20
 342 kGy. The swelling degree was found to be from 1.48 to 5.72.

343 **Characterization of the Alg-PAA/f-MWCNTs composite**

344 FTIR, SEM, XRD, TGA and DTA techniques were used to study and validate the
 345 structure of the composite. The Zeta potential and point of zero charge of the Alg-PAA/f-
 346 MWCNTs composite were also determined.

347 *Fourier-transform infrared analysis*

348 The FTIR spectrum of Alg-AA/f-MWCNTs composite showed the characteristic
 349 absorption band of Alg at 1116 cm^{-1} , typically of the stretching vibration of $-\text{C}-\text{OH}$
 350 (Figure 4a).



351

352 **Figure 4.** (a) The FTIR spectrum, and (b) TGA and DTA thermograms of Alg-PAA/f-
 353 MWCNTs composite.

354 The bands at 1424 cm^{-1} and 1459 cm^{-1} belong to the symmetric stretching of $-\text{COO}^-$
 355 group, while the band at 1559 cm^{-1} was assigned to the asymmetric stretching of $-\text{COO}^-$
 356 group of both Alg and AA. The absorption bands at 1741 cm^{-1} , 2854 - 2923 cm^{-1} , and
 357 3239 - 3612 cm^{-1} represented the asymmetric stretching vibration of $\text{C}=\text{O}$, $-\text{C}-\text{H}$, and -
 358 OH groups, respectively of the Alg, AA, and f-MWCNTs. The band at 1646 cm^{-1} denoted

359 the –C=C– stretching vibration of f-MWCNTs. These findings proved the efficient
360 grafting of the AA onto Alg/f-MWCNTs surface (**Figure 4a**).^[48-50]

361 *Thermal analysis*

362 **Figure 4b** shows the five-stages weight decomposition of Alg-PAA/f-MWCNTs. The
363 first weight loss until temperature of 200°C was found to be 4.7%, corresponding to
364 moisture loss. The second stage demonstrated the highest weight loss of 60.5% between
365 the temperature range 200 - 300°C, which might be associated with the breaking of the
366 main polymer chains. The third step with maximum temperatures at 335°C and 385°C,
367 corresponded to a total weight loss of 12.8% due to decarboxylation of polyacrylic acid
368 (PAA). The fourth stage with maximum temperatures at 460°C and 490°C exhibited a
369 weight loss of 10.1% due to chain fragmentation created by chains' scission. While the
370 last stage occurred at a temperature > 500°C with 10.9% weight loss for the f-MWCNTs
371 decomposition.

372 *X-ray diffraction analysis* The XRD pattern of Alg-PAA/f-MWCNTs composite showed
373 broad diffraction spectrum (**Figure S1; Supporting data**). It is known that Alg and PAA
374 have amorphous nature, while the f-MWCNTs exhibit two characteristic diffraction peaks
375 at 2θ values of approximately 26.0° and 43.9°, corresponding to the (002) and (100)
376 reflections, respectively.^[51] In this study, the XRD spectrum of Alg-PAA/f-MWCNTs
377 composite revealed three main humps at $2\theta = 20.15^\circ$, 31.23° , and 42.86° . The amorphous
378 nature of the Alg-PAA/f-MWCNTs was attributed to the non-crystalline character
379 induced by both Alg and PAA.^[52] The broad hump at $2\theta = 20.15^\circ$ may be related to
380 grafting of AA onto Alg/f-MWCNTs and destruction of the crystallinity, while the two
381 humps belong to the f-MWCNTs at $2\theta = 31.23^\circ$, and 42.86° showed slight shift from the
382 reported values, suggesting strong ionic interactions between the components of Alg-
383 PAA/f-MWCNTs composite.^[53]

384 *Particle size analysis*

385 Particle size and size distribution are important parameters for evaluating physical
386 stability, homogeneity, and the sedimentation rate of the nanoparticle suspension. The
387 particle size distribution of Alg-PAA/MWCNTs was measured through the polydispersity
388 Index (PDI) using DLS-Malvern Zeta sizer. The analysis showed a PDI value of 1.00 for
389 Alg-AA/MWCNTs, and the composite mostly has a uniform particles size of 150.7 nm
390 (**Figure S2; Supporting data**). This uniform distribution and small particles of Alg-
391 PAA/MWCNTs composite enable a larger surface area exposure for adsorption.^[54]

392 *Point of zero charge and Zeta potential analysis*

393 Zeta potential measurements are conducted to provide information about the surface
394 charge of Alg-PAA/f-MWCNTs composite. It has been reported that the pH_{pzc} of pristine
395 MWCNTs occurs at $\text{pH} = 3.7$, and the Zeta potential values are positive at $\text{pH} < \text{pH}_{\text{pzc}}$.^[55]
396 In the current study, the findings revealed that the isoelectric point (pH_{pzc}) of the
397 composite occurs at $\text{pH} = 6.28$ (**Figure S3a; Supporting data**). On the other hand, the
398 Zeta potential values of Alg-PAA/f-MWCNTs composite are negative (-12.00 to -30.2
399 mV) in the whole pH range, and the potentials become more negative as pH increases
400 from 2.0 to 12.0 (**Figure S3b; Supporting data**). The negative potentials agree with
401 previously reported values for functionalized-MWCNTs due to the added Alg and PAA
402 to the f-MWCNTs surface.^[55] These findings interpret the highest removal of the anionic
403 nigrosine dye by Alg-PAA/f-MWCNTs at $\text{pH} < \text{pH}_{\text{pzc}}$ reaching a maximum at $\text{pH} = 2.0$.
404 At pH values $< \text{pH}_{\text{pzc}}$ there is an elevation in the concentration of H^+ ions in the solution.
405 Consequently, the Alg-PAA/f-MWCNTs surface becomes protonated in an acidic
406 environment, leading to the formation of robust electrostatic forces of attraction between
407 the anionic nigrosine dye and function groups (e.g., -COOH, -OH) existing on the
408 adsorbent Alg-PAA/f-MWCNTs surface.^[56]

409 *Scanning electron microscopy*

410 The microstructure morphology and homogeneity of the Alg-PAA/f-MWCNTs
411 composite were inspected through the SEM analysis was done to inspect (**Figure 5**). The
412 SEM micrograph (**Figure 5b**) demonstrated a uniform and homogeneous of entangled
413 multilayered texture exhibiting holes with nearly equal radii distributed on the surface
414 compared with the micrograph of the Alg polymer (**Figure 5a**). These large continuous
415 interconnected layers create active sites which could increase the adsorption ability of the
416 dyes onto the composite's surface.

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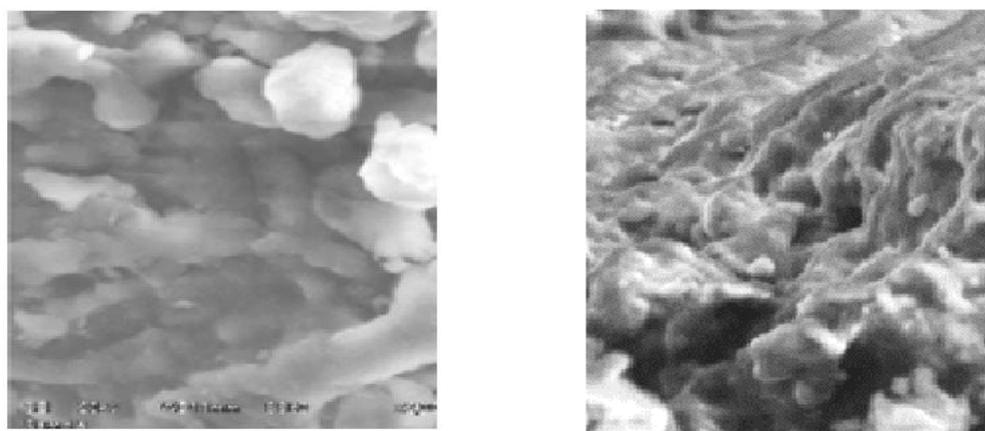
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424 **Figure 5.** SEM micrographs of (a) Alg polymer and (b) Alg-PAA/f-MWCNTs
425 composite.

426

427 *Adsorption performance of Alg-PAA/f-MWCNTs*

428 *Initial pH effect*

429 The removal of dye from aqueous solutions is highly pH dependent. A variation in pH
430 can influence the interactions between dye and adsorbents molecules due to the change
431 in the ionization level and surface charge of the absorbent. As a result, the impact of the
432 initial pH of the solutions on acid black II dye removal was investigated over a pH range
433 of (2.0 – 12.0) (**Figure 6a**). The data investigated that the maximum dye removal of
434 83.0% was observed at pH 2.0, then a significant decrease in dye removal was observed

435 by increasing the pH of the medium. The removal % was reduced significantly from
 436 32.0% at pH 3 reaching to 0% at pH 12, associated with increasing the electrostatic
 437 repulsion.

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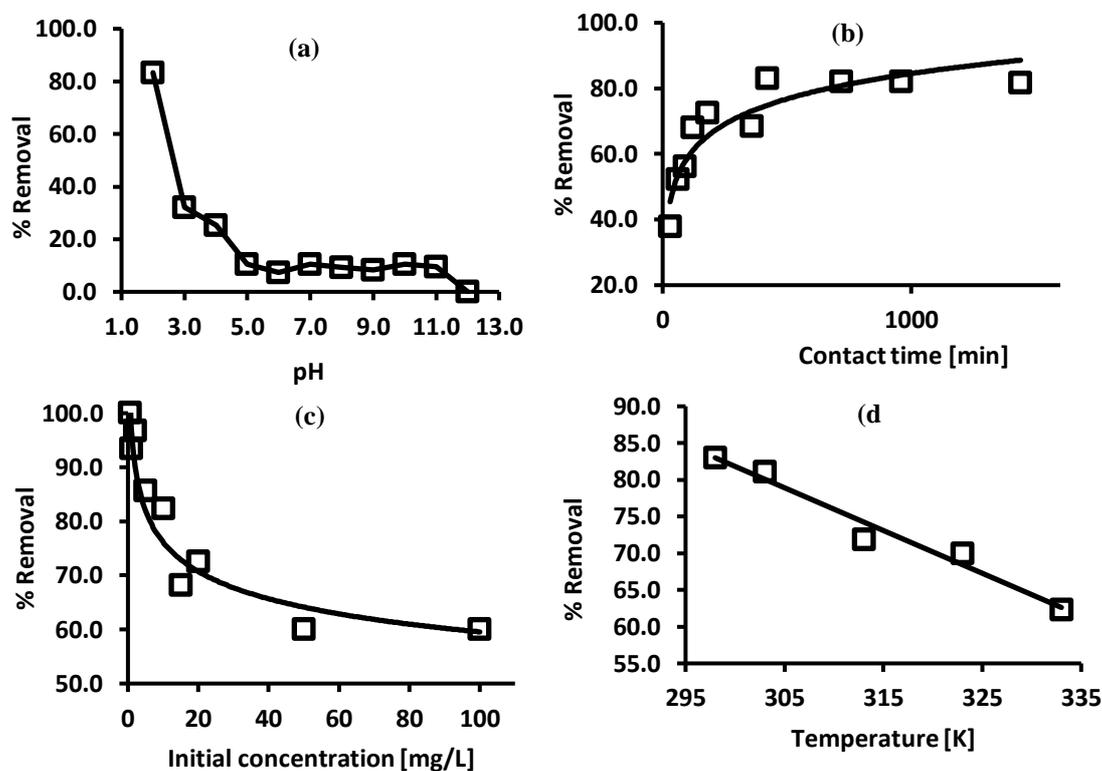
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452 **Figure 6.** Effect of (a) pH, (b) contact time, (c) initial dye concentration, and (d)
 453 temperature on the % removal of acid black II by Alg-PAA/f-MWCNTs adsorbent.

454

455 It has been reported that in an aqueous solution, acidic dye dissolves first, then
 456 dissociates, resulting in anionic dye ions.^[18, 57] At low pH most of the functional groups
 457 on the adsorbent surface such as $-\text{OH}$, $-\text{COOH}$, were protonated led to a significant
 458 electrostatic attraction for the anionic acid black II dye.^[58, 59] As the pH increases, the
 459 adsorption capacity decreased, which could be attributed to an increase in the number of
 460 negatively charged sites on the adsorbent surface, and hence a decrease in electrostatic
 461 attraction and competition for adsorption between acid black II dye and OH^- ions. In the
 462 current study, the pH value of 2.0 was selected as the optimum pH and used in the next

463 experiments with maximum removal of 83.0%. This finding matches with the observed
464 point of zero charge of the composite at $pH_{pzc} = 6.28$ (**Figure S3; Supporting data**),
465 below which the dye removal increases reaching the maximum at $pH = 2.0$ (**Figure 6a**).

466 *Effect of contact time*

467 Time of contact is a crucial parameter of consideration when designing a low-cost
468 wastewater treatment system ^[60]. The effect of contact time (30 – 1440 min) on the
469 adsorption was studied at the optimum pH conditions for the Alg-PAA/f-MWCNTs
470 composite. The results presented in **Figure 6b**, showed an optimum equilibrium time of
471 420 min was sufficient to attain equilibrium for adsorption of acid Black II onto Alg-
472 PAA/f-MWCNTs composite with the removal of 83.0% and maximum loading capacity
473 of 4.15 mg/g.

474 *Effect of initial dye concentration*

475 The influence of acid black II dye concentrations was investigated using the concentration
476 range 0.5 - 100 mg/L (**Figure 6c**). The highest removal (> 99.0%) was observed at lower
477 dye concentration (0.5-10 mg/L) may be attributed to the low (dye ion/binding sites) ratio.
478 As the concentration of dye increased, the adsorption ability decreased since all active
479 sites and the internal pores become saturated.^[61, 62]

480 *Influence of temperature*

481 The temperature has a significant effect on the adsorption mechanism because
482 temperature variations induce various changes in the adsorbent's equilibrium potential for
483 the adsorption of a certain adsorbate.^[63] Adsorption tests on Alg-PAA/f-MWCNTs
484 nanocomposite polymer were carried out at different temperatures (293, 303, 313, 323,
485 and 333 K), **Figure 6d**. The results indicated that the removal% of acid black II dye by

486 Alg-PAA/f-MWCNTs declined with increasing the temperature which highlights
487 exothermic adsorption.

488 ***Adsorption kinetics, isotherm, and thermodynamics***

489 *Adsorption kinetics studies*

490 The mechanism and rate of the adsorption process can be predicted based on kinetics
491 studies. Sorption kinetics of dye on the solid surface is usually explained as: the mass
492 transfer step when the dye molecules are rapidly transferred from the bulk solution to the
493 adsorbent surface, and a diffusion step in which dye molecules diffuse from the boundary
494 film of the sorbent into the inner active sites. The rate of diffusion step and dye adsorption
495 (K_{id}) is lower than the first step due to an increase in boundary layer film and a decrease
496 in vacant active sites accompanying the complexation, physicochemical sorption or ion
497 exchange processes. In the present study, the kinetics of adsorption were studied using
498 pseudo-first order, pseudo-second, and intra-particle diffusion models. For the adsorption
499 of acid back II on Alg-PAA/f-MWCNTs composite, the validity of the pseudo-first order
500 (Eq. 5), pseudo-second order (Eq. 6), and diffusion kinetics using Weber and Morris intra-
501 particle diffusion (Eq. 7) models, were checked.^[37] The perfectly suited model was
502 chosen according to the limit of compatibility between the calculated and experimental
503 (Q_e) values, as well as the linear correlation coefficient values (R^2).

504
$$\ln(Q_e - Q_t) = \ln Q_e - k_1 t \quad (\text{Eq. 5})$$

505
$$\frac{t}{Q_t} = \frac{1}{k_2 Q_e^2} + \frac{t}{Q_e} \quad (\text{Eq. 6})$$

506
$$Q_t = K_{id} t^{0.5} + C \quad (\text{Eq. 7})$$

507 Where, Q_e and Q_t are the adsorption capacity (mg/g) of adsorbents at equilibrium and at
508 time t (min), respectively. The k_1 (min^{-1}) and k_2 (g/mg/min) are the pseudo-first order and
509 pseudo-second order rate constant values, respectively. The K_{id} ($\text{mg/g/min}^{1/2}$) is the intra-
510 particle diffusion coefficient and C is the thickness of the boundary layer. The various

511 parameters were calculated by linear fitting the three models as shown in **Figures 7a-c**
 512 and **Table 1**.

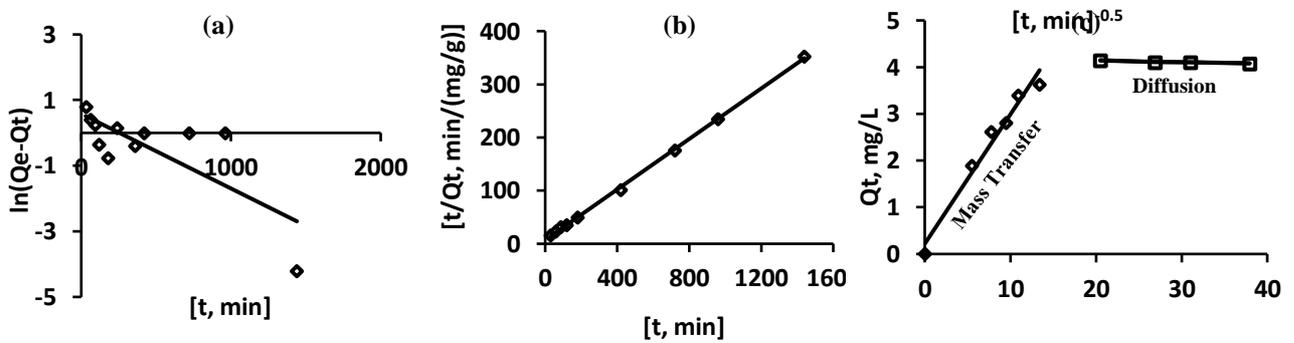
513 **Table 1.** Kinetic parameters for the sorption of acid black II on Alg-PAA/f-MWCNTs

$Q_e(\text{Exp.})$	Pseudo-first order			Pseudo-second order				Intra-particle diffusion		
	k_1	$Q_e(\text{Cal.})$	R^2	k_2	$Q_e(\text{Cal.})$	h	R^2	K_{id}	C	R^2
mg/g	min^{-1}	mg/g		g/mg/min	mg/g	$k_2 Q_e^2$		$\text{mg/g/min}^{1/2}$	-	
4.12	0.0023	1.78	0.577	0.0079	4.24	0.0936	0.999	0.0872	1.6592	0.714

514

515 Pseudo-second order has the highest R^2 (0.999) compared to other adsorption kinetic
 516 models, suggesting that the adsorption behaviour occurs mainly on the surface of Alg-
 517 PAA/f-MWCNTs, and controlled by the chemisorption mechanism (**Figure 7b**). The
 518 rate-limiting step is controlled by sharing or exchanging of electrons between the dye
 519 molecule and the adsorbate.

520



521

522 **Figure 7.** Kinetic plots for the sorption of acid black II over Alg-PAA/f-MWCNTs, (a)
 523 pseudo-first order model, (b) pseudo-second order, and (c) intra-particle diffusion
 524 models.

525

526 The calculated equilibrium adsorption capacity (Q_e) from pseudo-second order has values
 527 of 4.12 mg/g for acid black II sorption onto Alg-PAA/f-MWCNTs composite which are
 528 very close to the experimental values of 4.24 mg/g ($\Delta q = 0.12$). The pseudo-second order

529 rate constant (k_2) indicated that the adsorption process was achieved very fast. The intra-
 530 particle diffusion model (**Figure 7c**) showed two linear sections plots; thus the model
 531 cannot be accepted as the only rate-determining step. The first linear part in the model
 532 represents the mass transfer from solution to the solid surface ($R^2 = 0.971$) while the
 533 second part shows the diffusion of dye molecules from the surface to the inner layer (R^2
 534 $= 0.808$).

535 *Adsorption isotherms studies*

536 Three isotherm models were applied for studying the adsorption of acid black II on Alg-
 537 PAA/f-MWCNTs namely Freundlich (Eq. 8) ^[64], Langmuir (Eq. 9) ^[65], and Temkin (Eq.
 538 10) ^[66] models.

539

$$540 \quad Q_e = K_F C_e^{1/n} \quad \ln Q_e = \ln K_F + \frac{1}{n} \ln C_e \quad (\text{Eq. 8})$$

$$542 \quad \frac{1}{Q_e} = \frac{1}{bQ_m} \frac{1}{C_e} + \frac{1}{Q_m} \quad Q_e = \frac{Q_m bC_e}{1 + bC_e} \quad (\text{Eq. 9})$$

$$541 \quad Q_e = B_T (\ln K_T) + B_T (\ln C_e) \quad B_T = (RT)/b \quad (\text{Eq. 10})$$

543

544 B_T is Temkin constant $= RT/b$ (J/mol) and related to the heat of adsorption, while T is
 545 the absolute temperature (K); R is the ideal gas constant $= 8.314$ J/mol/K, and K_T is the
 546 equilibrium binding constant (L/min) related to the higher binding energy.

547 The adsorption of acid black II on Alg-PAA/f-MWCNTs has the highest R^2 (0.9601) with
 548 the Freundlich model compared to Langmuir ($R^2 = 0.816$), and Temkin ($R^2 = 0.625$),
 549 (**Figures 8a-c**) and (**Table 2**). This indicates that the adsorption mechanism is well fitting
 550 with the Freundlich isotherm model and the adsorption of acid black II on Alg-PAA/f-
 551 MWCNTs is closer to multi-layer adsorption with multiple adsorption sites (**Figure 8a**).
 552 The value of the Freundlich isotherm $0 < 1/n = 0.569 < 1$), indicating that the interaction
 553 between Alg-PAA/f-MWCNTs and dye molecules is strong, and the sorption process is
 554 likely to be favourable (**Table 2**).

555

556 **Table 2.** Isotherm parameters for the sorption of acid black II onto Alg-PAA/f-MWCNTs

557

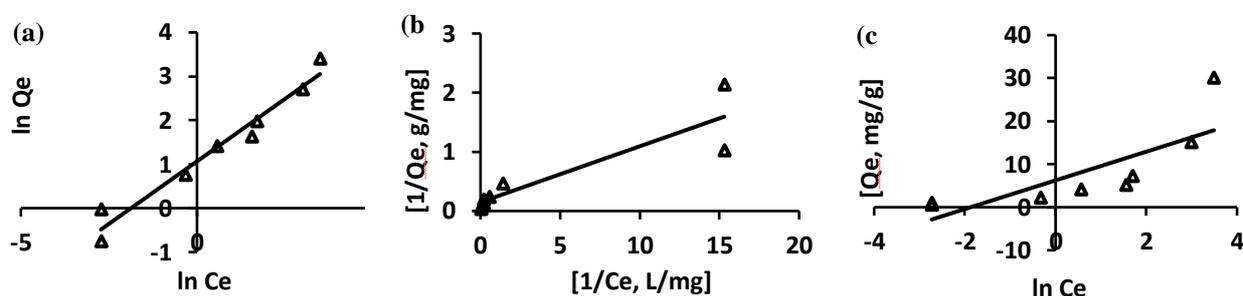
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	Freundlich	Langmuir	Temkin
n	1.757	Q_m 6.69	B_T 742.7
$1/n$	0.5691	b 1.7589	K_T 6.505
K_F	11.633		
R^2	0.9601	R^2 0.8164	R^2 0.6256

562 **Figure 8.** Isotherm plots for the sorption of acid black II on Alg-PAA/f-MWCNTs using

563 (a) Freundlich, (b) Langmuir, and (c) Temkin models.

564

565 However, the R^2 of Alg-PAA/f-MWCNTs for acid black II sorption using Langmuir

566 model close to 0.816, it was not fit with the known features of removal rate (i.e., high

567 removal at low concentration and low removal at high concentration), (**Figure 8b**) and568 (**Table 2**). This principle could be achieved using Freundlich model, the theoretical

569 adsorption capacity increased with increasing the initial concentration of the dye solution.

570 Thus, proved that the Freundlich adsorption model was more fitting for the adsorption of

571 acid black II on Alg-PAA/f-MWCNTs.

572 **Thermodynamic studies**573 Thermodynamic parameters including the changes in Gibbs free energy (ΔG^0 , kJ/mol),574 enthalpy change (ΔH^0 , kJ/mol), and entropy change (ΔS^0 , J/mol/K) were calculated from

575 the following equations (11 - 14).

$$576 \ln K_d = \frac{\Delta S^0}{R} - \frac{\Delta H^0}{RT} \quad (\text{Eq. 11})$$

577
$$K_d = \frac{Q_e}{C_e} \quad (\text{Eq. 12})$$

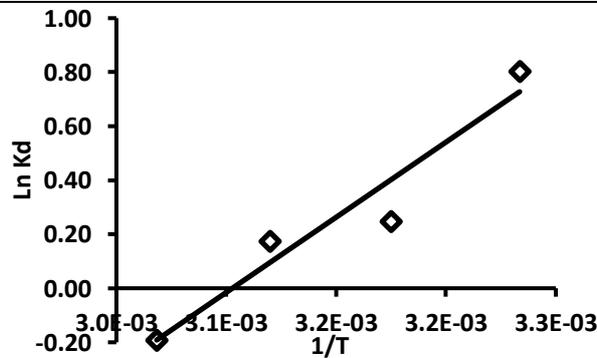
578
$$\Delta G^0 = \Delta H^0 - T\Delta S^0 \quad (\text{Eq. 13})$$

579
$$\Delta G^0 = -RT \ln K_d \quad (\text{Eq. 14})$$

580 Where R (8.314 J/mol/K) is the universal gas constant, T (K) is the absolute temperature
 581 and K_d is the distribution coefficient. The Linear plot of $\ln K_d$ versus $1/T$ for adsorption
 582 gives the slope and intercept equal to $(-\Delta H^0/R)$ and $(\Delta S^0/R)$, respectively. Indeed, the
 583 negative value of ΔG^0 confirmed the spontaneous nature and possibility of the adsorption
 584 via physical force. The results are summarized in **Table 3** and **Figure 9**. The sorption was
 585 random and thermodynamically favourable, as shown by the negative ΔG^0 values. Extra
 586 negative ΔG^0 indicated a stronger adsorption driving force, resulting in a higher sorption
 587 power. Furthermore, the negative value of the entropy ($\Delta S^0 = -78.76$) implied the decrease
 588 in the system's degree of freedom. The negative ΔH^0 value of (-17.850) in the case of acid
 589 black II sorption suggested exothermic adsorption.^[37]

590 **Table 3.** Thermodynamics parameters for acid black II adsorption on Alg-PAA/f-
 591 MWCNTs

T	ΔG^0	ΔH^0	ΔS^0
K	(kJ/mol)	(kJ/mol)	(J/mol/K)
303	-2.0211		
313	-0.6447	-25.699	-78.76
323	-0.4682		
332	0.5284		



592
 593 **Figure 9.** Thermodynamic plot for acid black II adsorption on Alg-PAA/f-MWCNTs
 594 composite.

595 ***Reusability of Alg-PAA/f-MWCNTs composite***

596 To evaluate the reusability of Alg-PAA/f-MWCNTs composite as adsorbent, five
597 sequential adsorption-desorption cycles were performed at the optimal conditions where
598 the adsorbed dye was rapidly desorbed in an alkaline medium. The effect of five reused
599 cycles on the adsorption capacity of Alg-PAA/f-MWCNTs (**Figure S4; Supporting**
600 **data**). It could be deduced that the adsorption capacity of Alg-PAA/f-MWCNTs
601 composite was above 80% after five-consecutive adsorption-desorption processes,
602 provoking the high-performance recyclability of the Alg-PAA/f-MWCNTs composite on
603 acid black II dye removal.

604 Comparison of the acid black II adsorption capacities of Alg-PAA/f-MWCNTs adsorbent
605 with other previously studied adsorbents is listed in **Table S1 (Supporting data)**. Based
606 on the results, the Alg-PAA/f-MWCNTs adsorbent is regarded as a promising adsorbent
607 and a good candidate for the removal of acid black II from wastewater.

608

609 The study concludes that an alginate-polyacrylic acid/multiwalled carbon nanotubes
610 (Alg-PAA/f-MWCNTs) composite was successfully prepared *via* gamma radiation-
611 induced template polymerization of AA onto Alg/f-MWCNTs surface. The maximum
612 grafting efficiency (GE%) of ~ 82% was obtained under optimized conditions of 2.5 wt%
613 Alg, 30 wt% AA, 0.5 wt% f-MWCNTs, 0.6 wt% *N,N'*-methylenebisacrylamide (NMBA),
614 and irradiation dose ~ 20 kGy. The structure and thermal characteristics of the prepared
615 composite were validated by FTIR, SEM, TGA, XRD, and DTA. The Alg-PAA/f-
616 MWCNTs composite exhibited uniform small particles size, with negative Zeta potentials
617 within the whole pH range of a minimum at pH = 2. The adsorption batch experiments
618 showed good adsorption capacity in the removal of the nigrosine dye from an aqueous
619 medium with adsorption efficiency of 83% . Adsorption of nigrosine dye onto the

620 composite was favourable thermodynamically obeying the Freundlich isotherm model
621 and controlled by chemisorption mechanism Interestingly, the composite showed a good
622 regeneration ability in the removal of the dye several times under the optimized
623 conditions. Accordingly, the Alg-PAA/f-MWCNTs composite could be a promising
624 candidate for the treatment of wastewaters from nigrosine dye.

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632

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634 **Conflict of interest:** The authors report there are no competing interests to declare.

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637

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639 Methods validation, Data curation and analysis, Writing and Reviewing. **Islam M.**
640 **Abdelmonem:** Conceptualization, Methodology, Data analysis, and Reviewing. **Laila.**
641 **A. Mohamed:** Conceptualization, Methodology, Methods validation, Data curation and
642 analysis, Writing and Reviewing. **Mohamed A. Gizawy:** Conceptualization,
643 Methodology, Data analysis and Reviewing. **Essam Metwally:** Conceptualization and
644 Reviewing.

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